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(54) Recovery of phosphorus from sludge.

(57) Elemental phosphorus is recovered from sludge by flash evaporation of the sludge utilizing a heat transfer means and separation of the phosphorus from the solid impurities contained in the sludge.

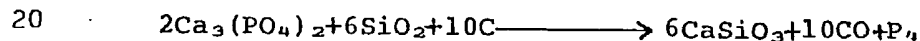
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RECOVERY OF PHOSPHORUS FROM SLUDGE

The present invention relates to an improved process for recovering elemental phosphorus from sludge, and more particularly from the sludge formed during the production of elemental phosphorus by the smelting of phosphate rock.

The basic method for producing elemental phosphorus is accomplished by the reduction of phosphate rock with coke or other carbonaceous reducing agents in the presence of silica. This is referred to as the furnace "charge" or "burden". The phosphorus production is generally carried out in an electric furnace at a reaction temperature of about 1,400° to about 1,500° C.

The mechanism of the reduction of phosphate rock to elemental phosphorus is quite complex and the exact path of the reaction sequence has not been conclusively defined. The overall reaction is generally represented by the following simplified equation:



During the course of the reaction, the phosphorus produced vaporizes, rises, and is cooled, condensed, and collected under water. The phosphorus vapor is generally accompanied by carbon monoxide and appreciable quantities of entrained dust comprising phosphate burden, fluorine, calcium oxides, potassium oxides and the like. The dust and vapor

mixture can be passed through an electrostatic precipitator where most of the dust is removed prior to cooling the phosphorus vapor. The CO gas can be recovered for use as fuel or properly
5 disposed of in accordance with pollution requirements. Solid furnace residue comprising calcium silicate is drawn off from the bottom of the furnace as a molten liquid. Iron phosphide or "ferrophosphorus" formed from the iron impurities
10 present in the phosphate ore is also drawn off as a melt from the bottom of the furnace.

The condenser drains into a sump wherein the phosphorus product is collected. Three separate layers generally form in the condenser sump.

15 A layer of relatively high grade phosphorus is obtained at the bottom. The intermediate layer is a mixture referred to as "sludge", which consists of phosphorus droplets or globules, solid impurities, and water. Above the sludge layer is a water layer.
20 The boundary between the sludge layer and water layer is not clearly defined.

The amount of phosphorus sludge (P_4 -sludge) produced will vary, depending upon factors such as the initial composition of phosphate rock charged,
25 the operating conditions and design of the furnace. Phosphorus sludge can contain from about 5% to about 90% by weight elemental phosphorus. The phosphorus content of the sludge produced can vary from about 10 to about 60 weight percent or more, of the furnace output of
30 elemental phosphorus.

The elemental phosphorus can be recovered from the sludge by roasting. This operation is becoming more expensive due to rising energy costs. It is also hazardous due to pressures
5 generated inside the roaster. In addition, roasting leads to high P_2O_5 emissions, a pollution problem. Other methods for treating the sludge include burning it and making low grade phosphoric acid.

10 The sludge, as the term is used in the art and herein, appears to be a poorly defined emulsion containing solid impurities, water and phosphorus in widely varying proportions and having a density between the density of phosphorus and the density
15 of water. The sludge can have the characteristics of a "phosphorus in water" type emulsion, that is, the phosphorus being the discontinuous phase and the water being the continuous phase, or a "water
20 in phosphorus" type emulsion, that is the water being the discontinuous phase and the phosphorus being the continuous phase. Microscopic examination of the phosphorus in water type sludge shows that the phosphorus is present in small globular part-
25 icles which will not coalesce. The size of the particles are generally in the range of micron to millimeter, and larger dimensions.

Various methods for recovering elemental phosphorus from sludge have been suggested in the
30 prior art. Among these are physical methods for separating the phosphorus, such as filtration, distillation, stirring and settling, vibration, centrifuging, extractions, electrolysis; and the like.

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U.S. Patent No. 3,104,952 to Hartig discloses a process of recovering elemental phosphorus from phosphorus sludge comprising admixing the sludge with phosphoric acid prior to or simultaneously with steam distillation. British Patent No. 524,289 discloses eliminating the water in the sludge by heating the sludge in a closed vessel under pressure below atmospheric, or to a temperature closely below the boiling point of water at atmospheric pressure for breaking the emulsion and causing the phosphorus to assume the form of a mobile melt from which solid impurities can be separated by any desired manner, as for instance, by filtering.

The present invention achieves the recovery of phosphorus from sludge by flash evaporating the water from the sludge utilizing a heat transfer means which eliminates the sludge.

In accordance with the invention elemental phosphorus is recovered from phosphorus sludge by a process comprising the steps of (1) flash evaporating the water from the sludge and (2) separating and recovering the elemental phosphorus from solid impurities contained in the evaporated sludge.

The invention therefore provides a process of recovering elemental phosphorus values from sludge particularly sludge derived from the production of elemental phosphorus comprising the steps of:

1. contacting the sludge with a heat transfer means at a temperature sufficient to flash evaporate

the water contained therein, and

2. recovering the elemental phosphorus values from the sludge.

In the practice of the invention water contained in the phosphorus sludge is flash evaporated causing the phosphorus to coalesce which thereby eliminates the sludge. As a result, the solid impurities in the phosphorus float to the surface resulting in the easy separation of the phosphorus from the solid impurities by well known techniques such as by centrifuging, filtering, settling or the like.

Heated phosphorus is utilized as a direct heat transfer fluid in the process for flash evaporating the water in the sludge. This process would eliminate the fouling and scaling problems associated with indirect heat transfer means such as heat exchangers, roasters and the like.

In the process, a sufficient amount of phosphorus is utilized with respect to the amount of sludge being treated to produce the preferred result of flash evaporating the water present and coalescing the phosphorus.

The solid impurities in the phosphorus which float to the surface when the sludge is eliminated generally comprised of phosphate, coke, hydrated and acidified alkalies from the furnace condensing operation.

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The process can be operated over a wide temperature range. Although it is only necessary to utilize a temperature high enough to evaporate the water, the temperature of the phosphorus, at atmospheric pressures, should be from 100°C to 110°C and preferably from 102°C to 105°C. In addition, flash evaporation can also be accomplished under vacuum or pressure at respectively lower or higher temperatures although pressures near atmospheric or higher are preferred.

10 An embodiment of the invention will now be described with reference to Figure I of the accompanying drawing which is a schematic illustration of the process. Referring to the drawing sludge is fed from a heated and stirred vessel 1 to a flash evaporator 2 by a metering system 3 via line 4. Various types of flash evaporators can be utilized in the process. The flash evaporator 2 in the embodiment is a heated and stirred vessel having a pump-around system 5 used primarily to reduce the size of the flash evaporator and the volume of "in process" phosphorus being circulated therefrom. The system 5 circulates and heats the phosphorus sludge in an external heat exchanger 6 via line 7 at a temperature above 100°C and generally at a temperature of from 105°C to 120°C. The sludge which may be preheated to 100°C is fed to the top of the flash evaporator 2 via line 8. The vapor, mainly water, from the flash evaporator 2 is used to preheat the sludge feed to the evaporator utilizing heat exchanger 9. The condensate from heat exchanger 9 which is contaminated with phosphorus is returned to the phosphorus condensing area as makeup water.

Alternatively, phosphorus may be recycled via line 10 if the concentration of solid impurities is too high for pumping.

5 It should be obvious that other methods of practicing the invention are within the knowledge of those skilled in the art. For instance, jacketed flash evaporator similar to 2, containing additional heating coils (not shown) can be utilized without a pump around system as shown in Fig. I.

10 In the embodiment shown the phosphorus and solid impurities are removed from the pump around system 5 by known means such as centrifuging, filtration, settling, represented by 11 and the like. The recovered solids which contain a small amount of phosphorus
15 can be recycled to the furnace, roasted or otherwise disposed of in an ecologically safe manner via line 12.

Claims:

1. A process of recovering elemental phosphorus values from sludge particularly sludge derived from the production of elemental phosphorus comprising the steps of:

1. contacting the sludge with a heat transfer means at a temperature sufficient to flash evaporate the water contained therein, and

2. recovering the elemental phosphorus values from the sludge.

2. A process as claimed in claim 1 characterised in that the heat transfer means is phosphorus.

3. A process as claimed in claim 2 characterised in that the phosphorus has a temperature of from 100 to 110°C.

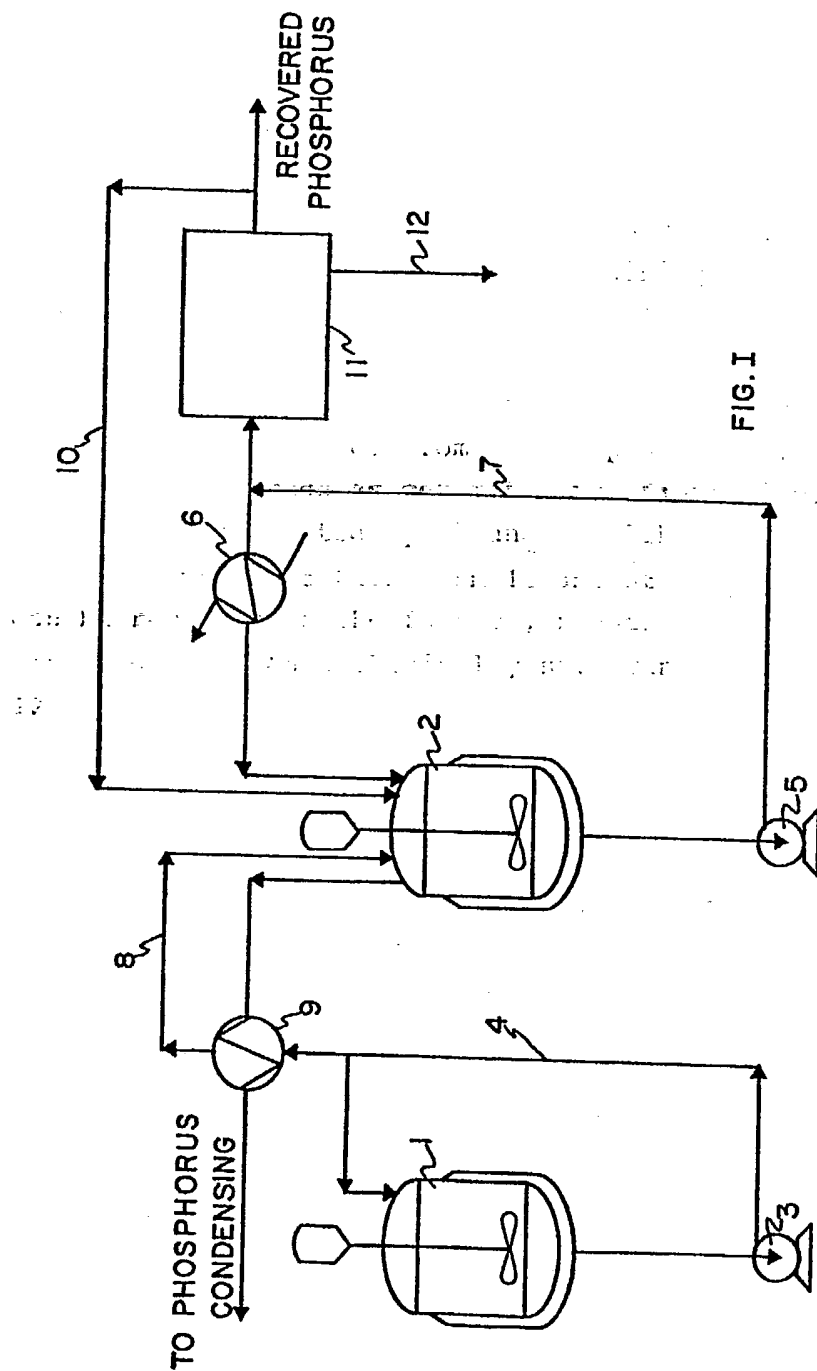


FIG. I



European Patent
Office

EUROPEAN SEARCH REPORT

0098038

Application number

EP 83 30 2598

DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl. 3)
A	GB-A- 801 246 (KNAPSACK-GRIESHEIM AG) * Claims 1, 2 *	1-3	C 01 B 25/02
A	US-A-3 084 029 (J.C. BARBER et al.) * Claim 1 *		
A	GB-A- 835 859 (KNAPSACK-GRIESHEIM AG) * Claim 1 *		
A	US-A-4 081 333 (W.S. HOLMES) * Claim 1 *	1	
D,A	GB-A- 524 289 (FARBENINDUSTRIE AG)		
D,A	US-A-3 104 952 (R.G. HARTIG et al.)		
			TECHNICAL FIELDS SEARCHED (Int. Cl. 3)
			C 01 B 25/01
			C 01 B 25/02
			C 01 B 25/02B
			C 01 B 25/027
The present search report has been drawn up for all claims			
Place of search BERLIN		Date of completion of the search 06-09-1983	Examiner ASSOGNA R.
<p>CATEGORY OF CITED DOCUMENTS</p> <p>X : particularly relevant if taken alone Y : particularly relevant if combined with another document of the same category A : technological background O : non-written disclosure P : intermediate document</p> <p>T : theory or principle underlying the invention E : earlier patent document, but published on, or after the filing date D : document cited in the application L : document cited for other reasons & : member of the same patent family, corresponding document</p>			